LISTING OF CLAIMS

Claims 1-7 (Cancelled)

8. (Amended) Process for the catalytic fluorination of saturated or olefinic halogenated hydrocarbons by HF in the gas phase, comprising flourination with ~~characterized in that~~ a catalyst based on chromium and on nickel which are obtained by impregnation of an amorphous chromium III oxide with a solution of a nickel derivative, characterized in that the chromium oxide used exhibits a BET specific surface of greater than 150 m^2/g and a pore volume of greater than 0.15 m1/g. ~~according to one of Claims 1 to 7 is used~~.

9. (Amended) Process according to Claim 8, wherein ~~in which,~~ before it is used, the catalyst is dried under an inert gas or under air at a temperature of between 100 and 350°C and then activated with HF.

10. (Amended) Process according to Claim 9, wherein ~~in which~~ the HF is first introduced diluted in air or, optionally ~~preferably~~, in an inert gas at a temperature ranging from 150 to 200°C and then pure at a temperature of less than 400°C~~, preferably of between 350 and 380°C~~.

11. (Amended) Process according to ~~one of Claims~~ Claim 8 ~~to 10~~, wherein ~~in which~~ the flourination temperature is between 50 and 500°C~~, preferably between 100 and 450°C and more particularly between 120 and 400°C~~.

12. (Amended) Process according to ~~one of Claims~~ Claim 8 ~~to 11~~, wherein ~~in which~~ the contact time is between 3 and 100 seconds~~, preferably less than 30 seconds~~.

13. (Amended) Process according to ~~one of Claims~~ Claim 8 ~~to 12~~, wherein ~~in which~~ the molar ratio: HF/halogenated hydrocarbon(s) is between 1/1 and 30/1~~, preferably less than 20/1~~.

14. (Amended) Process according to ~~one of Claims~~ Claim 8 ~~to 12~~, wherein ~~in which~~ the flourination is carried out at an absolute pressure of between 0.08 and 2 MPa~~, preferably between 0.1 and 1.5 MPa~~.

15. (Amended) Process according to ~~one of Claims~~ Claim 8 ~~to 14~~, wherein ~~in which~~ the flourination is carried out in the ~~present~~ presence of an oxidizing agent, optionally ~~preferably~~ oxygen or air.

16. (Amended) Process according to ~~one of Claims~~ Claim 8 ~~to 15~~, wherein ~~in which~~ the catalyst, deactivated by coking, is regenerated by treatment with air or with oxygen or by a Cl_2/HF mixture, at a temperature of between 250 and 400°C.

17. (Amended) Process according to ~~one of Claims~~ Claim 8 ~~to 16~~, wherein ~~in which~~ the halogenated hydrocarbon is perchloroethylene or 1-chloro-2,2,2-trifluoroethane.

18. (New) Process according to Claim 10, wherein the temperature is between 350 and 380°C.

19. (New) Process according to Claim 11, wherein the temperature is between 100 and 450°C.

20. (New) Process according to Claim 11, wherein the temperature is between 120 and 400°C.

21. (New) Process according to Claim 12, wherein the contact time is less than 30 seconds.

22. (New) Process according to Claim 13, wherein the molar ratio is less than 20/1.

23. (New) Process according to Claim 14, wherein the pressure is between 0.1 and 1.5MPa.